

11. ZADATAK

Procijeniti koeficijent kompresibilnosti i molarni volumen **ekvimolarne** smjese CO₂ i etana pri temperaturi od 250 K i tlaku od 10 atm. Pretpostaviti da se plinska smjesa pri tim uvjetima vlada prema Soave-Redlich-Kwongovom modelu.

Parametre smjese izračunati primjenom pravila miješanja, a polinomni oblik funkcije, $z=f(z)$, riješiti Newton-Gossetovim postupkom.

Podaci:

	T_K/K	p_K/atm	ω
CO₂(1)	304,2	73,8	0,225
etan(2)	305,4	48,8	0,099

unakrsni parametri: $k_{12}=k_{21}=0,1$

SOAVE REDLICH KWONG (1972)

Jednadžba

$$p = \frac{RT}{v-b} - \frac{a\alpha}{v(v+b)}$$

$$v^3 - \frac{RT}{p}v^2 - \left(b^2 + \frac{RTb}{p} - \frac{a\alpha}{p} \right)v - \frac{a\alpha b}{p} = 0$$

$$z^3 - z^2 - \left(\frac{b^2 p^2}{R^2 T^2} + \frac{bp}{RT} - \frac{a\alpha p}{R^2 T^2} \right)z - \frac{a\alpha b p^2}{R^3 T^3} = 0$$

$$z^3 - z^2 + (A - B^2 - B)z - AB = 0$$

Parametri

$$a = \frac{\Omega_a R^2 T_k^2}{p_k} \quad b = \frac{\Omega_b R T_k}{p_k}$$

$$\Omega_a = \frac{1}{9(2^{1/3} - 1)} = 0,427480 \quad \Omega_b = \frac{(2^{1/3} - 1)}{3} = 0,086640$$

$$\alpha = \left(1 + \kappa(1 - \sqrt{T_r}) \right)^2$$

$$\kappa = 0,48508 + 1,55171\omega - 0,15613\omega^2$$

$$\text{vodik: } \alpha = 1,202 \exp(-0,30288T_r)$$

$$A = \frac{a\alpha p}{R^2 T^2} = \frac{\Omega_a \alpha p_r}{T_r^2} \quad B = \frac{bp}{RT} = \frac{\Omega_b p_r}{T_r}$$

SMJESE REALNIH PLINOVA

Pravila miješanja

Soave-Redlich-Kwong

$$(a\alpha)_M = \sum_i \sum_j y_i y_j (a\alpha)_{ij}$$

$$b_M = \sum_i y_i b_i$$

$$A_M = \sum_i \sum_j y_i y_j A_{ij}$$

$$B_M = \sum_i y_i B_i$$

Dvokomponentne smjese

$$\begin{aligned}(a\alpha)_M &= (a\alpha)_{11} y_1^2 + (a\alpha)_{12} y_1 y_2 + (a\alpha)_{21} y_2 y_1 + (a\alpha)_{22} y_2^2 = \\ &= (a\alpha)_1 y_1^2 + 2(a\alpha)_{12} y_1 y_2 + (a\alpha)_2 y_2^2 \\ (a\alpha)_{11} &= (a\alpha)_1 \quad (a\alpha)_{22} = (a\alpha)_2 \quad (a\alpha)_{12} = (a\alpha)_{21}\end{aligned}$$

$$b_M = b_1 y_1 + b_2 y_2$$

Unakrsni parametri

Soave Redlich Kwong

$$(a\alpha)_{12} = (1 - k_{12}) \sqrt{(a\alpha)_1 (a\alpha)_2}$$

Zadatak:

CO₂(1) – ETAN(2)

$$T = 250 \text{ K}$$

$$p = 10 \text{ atm} = 1,013250 \text{ MPa}$$

$$y_1 = 0,5$$

Parametri a i b pojedinačnih fluida

$$a_1 = \frac{\Omega_a R^2 T_{K1}^2}{p_{K1}} = \frac{0,42748 \cdot 8,314^2 \cdot 304,2^2}{73,8 \cdot 101325} = 0,3657$$

$$b_1 = \frac{\Omega_b R T_{K1}}{p_{K1}} = \frac{0,08664 \cdot 8,314 \cdot 304,2}{73,8 \cdot 101325} = 2,93 \cdot 10^{-5}$$

$$a_2 = \frac{\Omega_a R^2 T_{K2}^2}{p_{K2}} = \frac{0,42748 \cdot 8,314^2 \cdot 305,4^2}{48,8 \cdot 101325} = 0,5574$$

$$b_2 = \frac{\Omega_b R T_{K2}}{p_{K2}} = \frac{0,08664 \cdot 8,314 \cdot 305,4}{48,8 \cdot 101325} = 4,449 \cdot 10^{-5}$$

Reducirane temperature pojedinačnih fluida

$$T_{r1} = \frac{T}{T_{K1}} = \frac{250}{304,2} = 0,8218 \quad T_{r2} = \frac{T}{T_{K2}} = \frac{250}{305,4} = 0,8186$$

Parametri κ pojedinačnih fluida

$$\begin{aligned}\kappa_1 &= (0,48508 + 1,55171\omega_1 - 0,15613\omega_1^2) = \\ &= (0,48508 + 1,55171 \cdot 0,225 - 0,15613 \cdot 0,225^2) = \\ &= 0,826311\end{aligned}$$

$$\begin{aligned}\kappa_2 &= (0,48508 + 1,55171\omega_2 - 0,15613\omega_2^2) = \\ &= (0,48508 + 1,55171 \cdot 0,099 - 0,15613 \cdot 0,099^2) = \\ &= 0,637169\end{aligned}$$

Parametri α pojedinačnih fluida

$$\begin{aligned}\alpha_1 &= [1 + \kappa_1 (1 - \sqrt{T_{r1}})]^2 = \\ &= [1 + 0,826311 (1 - \sqrt{0,8218})]^2 = 1,1604\end{aligned}$$

$$\begin{aligned}\alpha_2 &= [1 + \kappa_2 (1 - \sqrt{T_{r2}})]^2 = \\ &= [1 + 0,637169 (1 - \sqrt{0,8186})]^2 = 1,1247\end{aligned}$$

Pravila miješanja

$$(a\alpha)_{11} = 0,3657 \cdot 1,1604 = 0,4244$$

$$(a\alpha)_{22} = 0,5574 \cdot 1,1247 = 0,6269$$

$$\begin{aligned}(a\alpha)_{12} &= (1 - k_{12}) \sqrt{(a\alpha)_1 (a\alpha)_2} = \\ &= (1 - 0,1) \sqrt{0,4244 \cdot 0,6269} = 0,4642\end{aligned}$$

$$\begin{aligned}
(a\alpha)_M &= \sum_i \sum_j y_i y_j (a\alpha)_{ij} = \\
&= y_1^2 (a\alpha)_{11} + 2y_1 y_2 (a\alpha)_{12} + y_2^2 (a\alpha)_{22} = \\
&= 0,5^2 \cdot 0,4244 + 2 \cdot 0,5 \cdot 0,5 \cdot 0,4642 + 0,5^2 \cdot 0,6269 = \\
&= 0,4949
\end{aligned}$$

$$\begin{aligned}
b_M &= \sum_i y_i b_i = \\
&= y_1 b_1 + y_2 b_2 = 0,5 \cdot 2,93 \cdot 10^{-5} + 0,5 \cdot 4,449 \cdot 10^{-5} = \\
&= 3,6895 \cdot 10^{-5}
\end{aligned}$$

Parametri A i B smjese

$$A = \frac{(a\alpha)_M p}{R^2 T^2} = \frac{0,4949 \cdot 1013250}{8,314^2 \cdot 250^2} = 0,1160$$

$$B = \frac{b_M p}{R^2 T^2} = \frac{3,6895 \cdot 10^{-5} \cdot 1013250}{8,314 \cdot 250} = 0,0180$$

Newton-Gosset (SRK)

$$f(z) = z^3 - z^2 + (A - B^2 - B)z - AB$$

$$f'(z) = 3z^2 - 2z + (A - B^2 - B)$$

Početne pretpostavke:

$$z^V = 1 \quad z^L = B$$

$$z^{(0)} = 1 \quad z^{(0)} = 0,018$$

$$z^{(1)} = 0,912918 \quad z^{(1)} = 0,0283435$$

$$z^{(2)} = 0,89413 \quad z^{(2)} = 0,0306501$$

$$z^{(3)} = 0,893272 \quad z^{(3)} = 0,030774$$

$$z^{(4)} = 0,89327 \quad z^{(4)} = 0,0307744$$

$$z^{(5)} = 0,89327 \quad z^{(5)} = 0,0307744$$

$$v^V = \frac{z^V RT}{p} = \frac{0,89327 \cdot 8,314 \cdot 250}{1013250} = 1,83238 \cdot 10^{-3} \text{ m}^3 \text{ mol}^{-1}$$

$$v^L = \frac{z^L RT}{p} = \frac{0,0307744 \cdot 8,314 \cdot 250}{1013250} = 6,31281 \cdot 10^{-5} \text{ m}^3 \text{ mol}^{-1}$$

